

Amendments to the Claims:

This listing of claims will replace all prior versions and listings of claims in the application:

Listing of Claims:

1. (withdrawn) A plant comprising:
a first shift reactor and a second shift reactor, wherein the first shift reactor is configured to receive a first portion of a syngas from a gasification unit or a partial oxidation unit and to form a first shift reactor effluent;
wherein the second shift reactor is configured to receive a combination of the first shift reactor effluent and a second portion of the syngas to form a second shift reactor effluent; and
wherein a temperature of the first portion and a temperature of the combination of the first shift reactor effluent and the second portion of the syngas are about the same.
2. (withdrawn) The plant of claim 1 wherein the second portion of the syngas is combined with the first shift reactor effluent in an amount effective to reduce steam demand by at least 10%.
3. (withdrawn) The plant of claim 2 wherein the second portion of the syngas is combined with the first shift reactor effluent in an amount effective to reduce steam demand by at least 35%.
4. (withdrawn) The plant of claim 1 further comprising a humidifier coupled to the first shift reactor, wherein the syngas is humidified in the humidifier before entering the first shift reactor, and wherein the second portion of the syngas is combined with the first shift reactor effluent in an amount effective to reduce water consumption of the humidifier by at least 20%.
5. (withdrawn) The plant of claim 1 wherein the second portion has a volume of between 50 vol% to 75 vol% of the syngas from the gasification unit or partial oxidation unit.

6. (withdrawn) The plant of claim 1 further comprising a bypass that combines a third portion of the syngas with the second shift reactor effluent.
7. (withdrawn) The plant of claim 1 wherein the syngas includes carbon monoxide and hydrogen in a molar ratio of at least 2:1.
8. (withdrawn) The plant of claim 1 further comprising an acid gas removal unit that is coupled to the second shift reactor and that removes carbon dioxide from the second shift reactor effluent.
9. (currently amended) A method of reducing steam consumption in a plant comprising a first shift reactor and a second shift reactor, comprising:
splitting a syngas from a gasification unit or a partial oxidation unit into a first portion and a second portion;
combining only the first portion with steam sufficient to support a shift reaction to form a steam-containing first portion, wherein the steam is the only source of water added to the first portion, and feeding the steam-containing first portion to the first shift reactor to form a first shift reactor effluent;
bypassing the second portion around the first shift reactor and combining the first shift reactor effluent with the second portion to form a mixed feed gas, and reacting the mixed feed gas in the second shift reactor to form a second shift reactor effluent;
obtaining data that indicate that when ~~wherein~~ the second portion is combined with the first shift reactor effluent, in an amount effective to reduce steam consumption in the first and second shift reactors and condensate formation in the second shift reactor effluent is reduced as compared to a plant operating without the step of bypassing the second portion around the first shift reactor;
operating the first and second shift reactors at about the same temperature.
10. (Original) The method of claim 9 wherein the second portion of the syngas is combined with the first shift reactor effluent in an amount effective to reduce steam demand by at least 10%.

11. (Original) The method of claim 9 wherein the second portion of the syngas is combined with the first shift reactor effluent in an amount effective to reduce steam demand by at least 35%.
12. (Original) The method of claim 9 wherein the second portion has a volume of between 50 vol% to 75 vol% of the syngas from the gasification unit or partial oxidation unit.
13. (Original) The method of claim 9 further comprising providing a bypass that combines a third portion of the syngas with the second shift reactor effluent.
14. (Original) The method of claim 9 wherein the syngas includes carbon monoxide and hydrogen in a molar ratio of at least 2:1.
15. (Original) The method of claim 9 further comprising coupling an acid gas removal unit to the second shift reactor, and removing carbon dioxide from the second shift reactor effluent in the acid gas removal unit.